



Casting Emission Reduction Program

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Core Manufacturing Process Variables Study Part II – Core Making (Blowing)

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UNITED STATES COUNCIL FOR AUTOMOTIVE RESEARCH

DAIMLERCHRYSLER *Ford Motor Company* General Motors

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Executive Summary

The objective of this testing was to determine the emission levels from the core making process for the CERP standard phenolic urethane (PU) binder system. During the core-blowing portion of the test, the gassing and purge emissions and the “fugitive” emissions were measured together. For this study, thirty (30) core blowing events of approximately thirty (30) minutes were established as a sample run.

The core blowing was conducted within an enclosure meeting the criteria for a temporary total enclosure (TTE) as specified in US EPA Method 204. Samples for Hydrocarbon Content (HC) as Hexane were collected on sorbent tubes during each run for subsequent laboratory analysis in accordance with an approved Wisconsin DNR method. All sampling locations were consistent with US EPA Method 1. US EPA Method 25A, Total Gaseous Organic Concentration (TGOC), was used to monitor all segments of the test, but was not reported due to the predominance of the triethylamine catalyst.

Process variables (sand temperature, binder content, blow time, blow pressure, purge air pressure, purge air temperature, purge duration, and sand particle size) were evaluated regarding their influence on the air borne emissions. The emissions evolved during this part of the experiment come from sand materials previously subjected to the same seven (7) minute mixing criteria described in Part I: Mixing of this three part report. Testing was done in a Redford/Carver Model CB22 vertical core machine. The test piece was a standard 1-on, 7.25 pound, AFS step core

The major emissions from the PU binders were caused by the evaporation of the solvents from the resin. The core blowing process includes all three physical parameters influencing evaporation: temperature, effective exposed surface area, and air movement over the surface of the coated sand grains.

Core making by mechanized blowing is a multi-step set of processes. The previously mixed sand is pneumatically injected into the core box causing the sand surface to be momentarily increased several fold. Heated blow air permeates the liquid-coated, initially loose, granular mass. Once in place the liquid binder components are cured into a rigid mass by percolation of the catalyst triethylamine (TEA). Heated purge air removes most of the volatile solvents and the toxic catalyst TEA by permeating the geometrically fixed solid core. Some of the volatile solvents are retained on internal sand surfaces while others are temporarily trapped in the rigid binder and are carried with the core to storage.

The primary emission parameters were demonstrated to be the mean sand particle size (GFN), the blow duration, and the sand temperature. As was learned in the Mixing section, (Part I) of this report, the sand temperature is the primary driver for the evaporation process. The blow time reflects the duration of time when the sand is loosely aggregated and when air can freely pass through the sand contacting most of the coated surface to purge emissions. The core, once formed, has much less apparent surface area.

The ability of the purge air to pass through the core and scavenge emissions is dependent on the open voids between the sand grains. The sand particle sizing and distribution defines the open voids. The higher the mean particle size, GFN, the more resistance to air is passing through the core. Secondary drivers were identified to be all of the other above mentioned measured parameters because of their influence on the air movement over and through the sand and thus determining the amount of apparent exposed surface. The sand surface is both the core surface and the inter-granular voids.

The table below illustrates the relative total emissions measured resulting from variation of the parameters during core blowing. The table is ranked by influence and correlation confidence. The negative sign in the relative emissions column indicates a reduction in emissions with an increase in parametric value.

Core Making Process Event	Core Making Regression Equation, HC as Hexane Emission x 10	Correlation Coefficient, R ²	Relative Make Emission Change Over the Parameter Range
Sand Mean Particle Size, GFN	$Y = 0.0008 X^2 - 0.143X + 7.99$	0.85	-11.6
Blow Time, Seconds	$Y = 0.065 X + 2.44$	0.75	3.7
Sand Temperature, F	$Y = 0.0065 X + 2.28$	0.60	2.3
Binder Content, %	$Y = 0.14 X + 2.50$	0.35	1.0
Purge Temperature, F	$Y = 0.0065 X + 0.79$	0.13	3.8
Purge Pressure, psi	$Y = 0.0082 X + 2.37$	0.09	2.7
Purge Time, Seconds	$Y = 0.011 X + 2.41$	0.19	2.1
Blow Pressure, psi	$Y = 0.0036 X + 2.68$	0.16	1.0

It must be noted that the reference and product testing performed is not suitable for use as emission factors or for purposes other than evaluating the relative emission reductions associated with the use of alternative materials, equipment, or processes. The emissions measurements are unique to the specific castings produced, materials used, and testing methodology associated with these tests, and should not be used as the basis for estimating emissions from actual commercial foundry applications.

1.0 Introduction

1.1 Background

Technikon LLC is a privately held contract research organization located in McClellan, California, a suburb of Sacramento. Technikon offers emissions research services to industrial and government clients specializing in the metal casting and mobile emissions areas. Technikon operates the Casting Emission Reduction Program (CERP). CERP is a cooperative initiative between the Department of Defense (US Army) and the United States Council for Automotive Research (USCAR). Its purpose is to evaluate alternative casting materials and processes that are designed to reduce air emissions and/or produce more efficient casting processes. Other technical partners directly supporting the project include: the American Foundry Society (AFS); the Casting Industry Suppliers Association (CISA); the US Environmental Protection Agency (US EPA); and the California Air Resources Board (CARB).

1.2 CERP Objectives

The primary objective of CERP is to evaluate the impact of new materials, equipment, and processes on airborne emissions from the production of metal castings. To accomplish this objective, the Technikon facility has been created to evaluate alternate materials and production processes designed to achieve significant airborne emission reductions, especially for organic Hazardous Air Pollutants (HAPs). HAP emissions reduction from the alternative materials, equipment and production processes is expressed as a comparison to similar emissions from a baseline or reference test. The facility has two principal testing arenas: a Pre-Production Foundry designed to measure airborne emissions from individually poured molds, and a Production Foundry designed to measure air emissions in a continuous, full-scale production process. Each of these testing arenas has been specifically designed to facilitate the collection and evaluation of airborne emissions, and associated process data. Candidate materials and/or processes are screened for emission reductions in the Pre-production Foundry and then further evaluated in the Production Foundry. The data collected during the various testing projects are evaluated to determine the impact of the alternate materials and/or processes on airborne emissions as well as on the quality and economics of casting and core manufacture. These alternate materials, equipment, and processes may need to be further adapted and defined so that they will integrate into current commercial green sand casting facilities smoothly and with minimal capital expenditure.

Pre-production testing is conducted in order to evaluate the impact on air emissions from a proposed alternative material, equipment or process. The Pre-Production Foundry is a simple, general-purpose manual foundry, which was adapted and instrumented to allow the collection of detailed emission measurements, using methods based on USEPA air testing protocols. Measurements are taken during pouring, casting cooling, and shakeout processes performed on discrete mold and core packages under tightly controlled conditions not feasible in a commercial foundry.

Alternative materials, equipment and processes that, during their testing in the Pre-Production Foundry, demonstrate significant air emission reduction potential and preserve casting quality

parameters are further evaluated in the Production Foundry. The Production Foundry's design as a basic green sand foundry was deliberately chosen so that whatever is tested in this facility could be easily converted for use in existing mechanized commercial foundries. The Production Foundry emulates an automotive foundry in the type and size of equipment, materials, and processes used. A single cavity automotive I-4 engine block mold is used to further evaluate materials, equipment, and processes in a continuous real-world production-like environment. The Production Foundry provides simultaneous, detailed, individual emission measurements, according to methods based on US EPA air testing protocols, of the melting, pouring, sand preparation, mold making, and core making processes. The Production Foundry is instrumented so that process data on all activities of the metal casting process can be simultaneously and continuously collected in order to complete an economic impact evaluation of the prospective emission reducing strategy. Castings are randomly selected to evaluate the impact of the alternate material, equipment, or process on the quality of the casting.

Test results for a particular process or product may not be the same from both foundries due to differences in the testing process. The Pre-production Foundry is designed to screen new products, processes, or equipment, whereas the Production Foundry is designed to test the effect of the product, process, or equipment in a continuous production-like environment.

The results of the testing conducted at both the Production and Pre-production Foundries are not suitable for use as general emission factors. The specific materials used (gray iron from an electric melt furnace, greensand with seacoal, and a cold box core with a relatively old resin binding system); the specific castings produced the specific production processes employed (a stationary hand-poured mold in the Pre-production Foundry and an impact mold line in the Production Foundry); and the specific testing conditions (relatively low stack velocity, long sampling times, high capture rates, and combined emissions from pouring, cooling and shakeout processes at the Production Foundry) produce emission results unique to the materials, castings, casting processes and measurement conditions used. The data produced are intended to demonstrate the relative emission reductions from the use of alternative materials, equipment and processes, and not the absolute emission levels that would be experienced in commercial foundries. A number of process parameters such as casting surface area, sand to metal ratios, pouring temperatures, stack flow rates, LOI levels, seacoal and resin contents, and the type of foundry (Cope & Drag versus Disa for example) can have a significant impact on actual emission levels.

The Production Foundry provides simultaneous detailed individual emission measurements using methods based on US EPA protocols for the melting, pouring, sand preparation, mold making, and core making processes. The core making area of the Production foundry contains three core blowers, a Georg Fischer for the preparation of automotive block cores, a Redford that is used for the production of step cores, and a second smaller Redford to produce dogbone tensile test specimens.

1.3 Report Organization

This report has been designed to document the methodology and results of a specific test plan that was used to evaluate the variability of emissions from the core mixing, making and storage

process. Separate reports will be issued to document the same information from the Core Making and Storage processes. Section 2 of this report includes a summary of the methodologies used for data collection and analysis, emission calculations, QA/QC procedures, and data management and reduction methods. Section 3 presents the results of the experimentation. Section 4 of this report contains a discussion of the results.

The raw data for this test series are included in a data binder that is maintained at the Technikon facility.

1.4 Specific Test Plan and Objectives

This Part II report contains the results of testing performed to provide data on selected emissions from the core sand making processes. Core mixing and core storage results will be reported in Parts I and III of this study. The table below provides a summary of the test plan for Test EU. The details of the approved test plan are included in Appendix A.

Test Plan Summary

	Test EU
Type of Process Tested	Core Sand: Part I - Mixing Part II - Core Making (Blowing) Part III - Core Storage
Test Plan Number	1409 – 131
Binder System	Phenolic Urethane Cold Box Ashland Isocure® 905/304
Number of Tests	13 at Core Mixing (Part I); 51 at Core Making (Part II); 51 at Core Storage (Part III)
Test Dates	11/13/02 through 1/22/03
Emissions Measured	TGOC as Propane (Part I), HC as Hexane (Parts II & III)
Process Parameters Measured	Process Sand Weight; Sand and Ambient Air Temperature; Binder Concentration; Mixer Cycle Time, Loading, Speed, & Ventilation; Core Blower Cycle Time and Blow & Purge Air Pressure, Air Temperature, & Duration.
Source Parameters Measured	Mixer, Core Blower Enclosure, & Storage Enclosure Exhaust Duct Temperature, Pressure and Volumetric Flow Rate

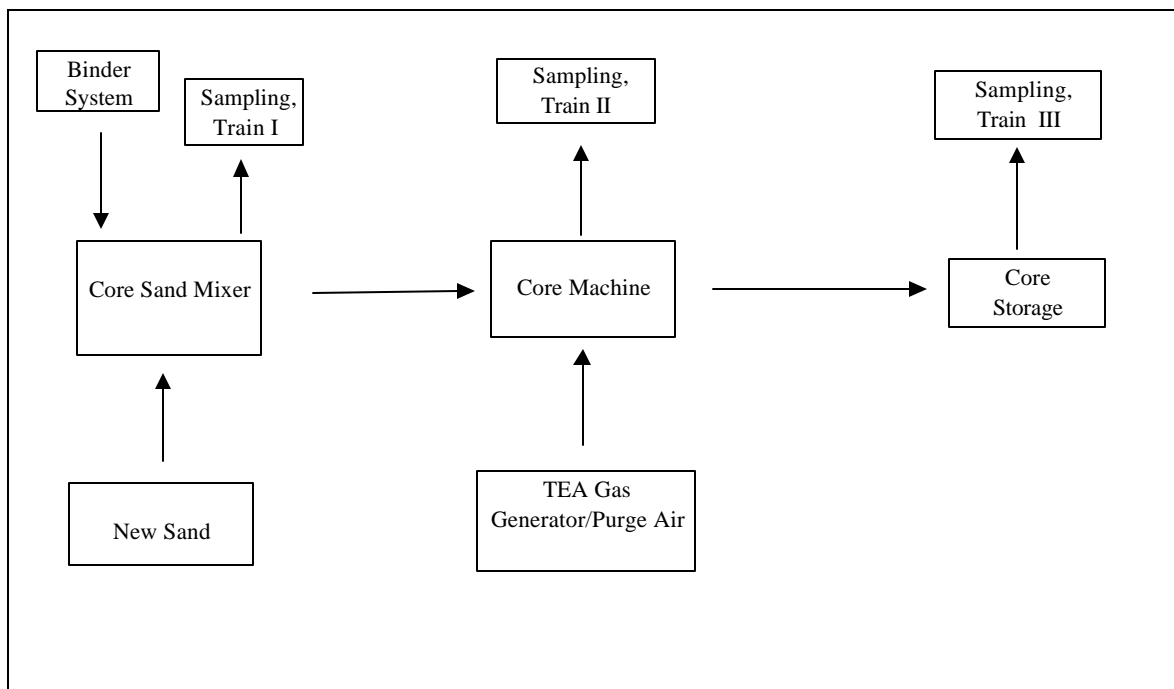
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2.0 Test Methodology

2.1 Description of Process and Testing Equipment

Figure 2-1 is a diagram of the Phenolic Urethane Cold box core making process and testing equipment.

Figure 2-1 Core Making and Testing Process



2.2 Description of Testing Program

The specific steps used in this sampling program are summarized below:

1. **Test Plan Review and Approval:** The proposed test plan was reviewed by the Technikon staff and the CERP Steering Committee, and approved.
2. **Sand Preparation:** Sands are mixed with quantities of designated binders in a covered 50-pound capacity paddle type cylindrical mixer qualifying as a temporary total enclosure, meeting US EPA Method 204 criteria. The sand is preheated or cooled as required to a standard

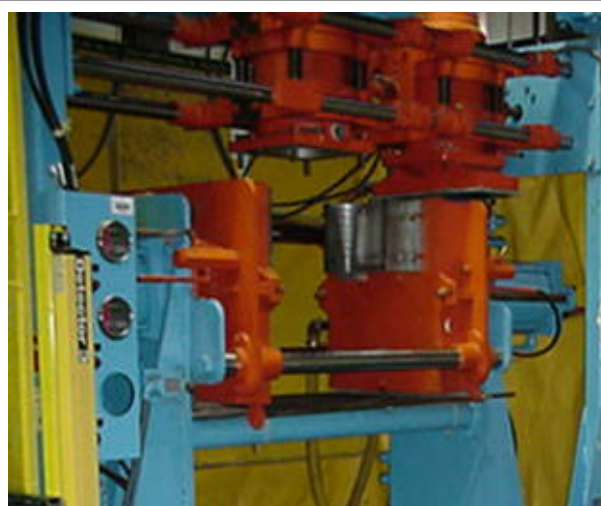
temperature range. The mixer is continuously bathed in temperature-controlled air to maintain the process temperature. Weighed sand and binder components are introduced via an openable window in the cover and mixed for a designated period of time, then discharged. The cycle time is determined to maintain continuous mixing activity while providing a balanced supply of sand to the core making operation.

3. **Core Preparation:** Step cores were prepared for this test in the Production foundry core room area. The sand and binder were mixed and then introduced (blown) into the core tooling of the Redford-Carver core machine. The core-making machine was contained in a permanent total enclosure meeting US EPA Method 204 criteria. An aliquot of the catalyst triethylamine (TEA) gas was heated to 84°F and allowed to expand into the piping leading to the core box. Finally, purge air, heated to 80°F, pushed the catalyst into the sand in the core box to cure the core, then flushed the catalyst from the core. All these gases were exhausted to a wet gas scrubber charged with sulfuric acid at pH 2 or less. Step cores were fabricated in a single cavity core box. One blow produces a single step core.



*Sand Mixing
(Enclosure not shown)*

4. **Individual Sampling Events:** Sampling to determine the core making emissions consisted of two (2) segments. During the production of step cores, air samples were collected to determine the amount of solvent vented off of the core process. The samples were collected after the background had stabilized during each of the thirty (30) core runs that comprised this portion of the test.



*Core Making
(Enclosure not shown)*

All of the enclosures used during this test meet or exceed US-EPA Method 204 criteria for Temporary Total Enclosures.

5. **Parameter Measurements:** Table 2-1 lists the process parameters that are monitored during each test. The analytical equipment and methods used are also listed.

Table 2-1 Process Parameters Measured

Parameter	Analytical Equipment and Methods
Binder Weight (mixing)	Mettler PJ8000 Digital Scale (Gravimetric)
Core Sand Weight (mixing)	Simpson IQ-800-3A Digital Scale
Sand Temperature (mixing)	Stem type dial thermometer & thermocouple
Sand Temperature (blowing)	Thermocouple
Cycle Time	Digital elapsed time clocks
Purge & Blow Air Temperature	Thermocouple
Purge & Blow Air Pressure	Digital & analog pressure gauges
Enclosure Air Temperature	Thermocouple
TEA Weight	Mettler PB302 Scale (310 gm)
Step Core Weight	OHAUS 110# digital platform scale

6. **Air Emissions Analysis:** The specific sampling and analytical methods used in the core sand mixing, making, and core storage tests are based on the US EPA reference methods shown in Table 2-2. The details of the specific testing procedures and their variance from the reference methods, if any, are included in the Technikon Standard Operating Procedures.

Table 2-2 Sampling and Analytical Methods

Measurement Parameter	Test Method*
Port location	EPA Method 1
Number of traverse points	EPA Method 1
Gas velocity and temperature	EPA Method 2
HC as Hexane,	NIOSH 1500,
TGOC (THC) as Propane	EPA Method 25A

* These methods were specifically modified to meet the testing objectives of the CERP Program.

Data Reduction, Tabulation and Preliminary Report Preparation: The analytical results of the emissions tests provide the mass of each analyte in the sample. For the core-blowing segment of the test, the total mass of the analyte emitted is calculated by multiplying the mass of analyte in the sample times the ratio of the sample volume to the total stack gas volume during the test. The total stack gas volume is calculated from the measured stack gas velocity and duct diameter. The total mass of analyte is then related to the varied process parameter.

7. **Report Preparation and Review:** The Preliminary Draft Report is reviewed by the Manager, Process Engineering, and the Emissions Team to ensure its completeness, consistency with the test plan, and adherence to the prescribed QA/QC procedures. Appropriate observations, conclusions and recommendations are added to the report to produce a Draft Report. The Draft Report is reviewed by the Vice President-Measurement Technologies, the Vice President-Operations. Comments are incorporated into a Final Report prior to final signature approval and distribution.

2.3 Quality Assurance and Quality Control (QA/QC) Procedures

Detailed QA/QC and data validation procedures for the process parameters, stack measurements, and laboratory analytical procedures are included in the Technikon Standard Operating Procedures. In order to ensure the timely review of critical quality control parameters, the following procedures are followed:

- Immediately following the individual sampling events performed for each test, specific process parameters are reviewed by the Manager - Process Engineering to ensure that the parameters are maintained within the prescribed control ranges. Where data are not within the prescribed ranges, the Manager - Process Engineering and the Vice President-Operations determine whether the individual test samples should be invalidated or flagged for further analysis following review of the laboratory data.
- The source (stack) and sampling parameters, analytical results and corresponding laboratory QA/QC data are reviewed by the Emissions Measurement Team to confirm the validity of the data. The VP-Measurement Technologies reviews and approves the recommendation, if any, that individual sample data should be invalidated. Invalidated data are not used in subsequent calculations.

3.0 Test Results

Figure 3-1 shows the variation in emissions as Hexane derived from silica sands that have mean particle sizes(GFN) of 50, 70 , & 90 equivalent US sieve sizes.

Figure 3-2 shows the variation in emissions as Hexane derived from Lake sand cores blown at 2, 5, & 8 seconds.

Figure 3-3 shows the variation in emissions as Hexane derived from Lakesand cores made with sands at 63, 82 & 100 degrees Fahrenheit.

Figure 3-4 shows the variation in emissions as Hexane derived from Lakesand cores containing 1.00 & 1.75 % Phenolic Urethane binder.

Figure 3-5 shows the variation in emissions as Hexane derived from Lakesand cores made with the purge temperature varied from 171 to 232 degrees Fahrenheit.

Figure 3-6 shows the variation in emissions as Hexane derived from Lakesand cores made as the purge pressure was varied from 22 to 57 psi.

Figure 3-7 shows the variation in emissions as Hexane derived from Lakesand core made as the purge time was varied from 10 to 30 seconds.

Figure 3-8 shows the variation in emissions as Hexane derived from Lakesand cores made as the blow pressure was varied from 15 to 45 psi.

Table 3-2 Process Regression Equations and Relative Impact on Emissions

Table 3-1 Weight of Emissions as Hexane Recovered from 30 Cycle Core Blowing Process.

Core Making Parameter	Parameter Value	Emission Weight Recovered as Hexane, pounds
Sand Mean Particle Size, GFN	50	0.283
	70	0.188
	95	0.158
Blow Time, Sec	2	0.253
	5	0.283
	8	0.252
Sand Temperature, F	63	0.268
	82	0.283
	100	0.292
Binder Content, %(BOS)	1.00	0.264
	1.75	0.274
Purge Temperature, F	171	0.217
	181	0.138
	201	0.251
	232	0.219
Purge Pressure, Psi	22	0.241
	32	0.283
	57	0.276
Purge Time, Sec	10	0.242
	20	0.283
	30	0.276
Blow Pressure	15	0.271
	32	0.283
	45	0.272

Figure 3-1 Total Emission from Core Making vs. Sand Particle Size

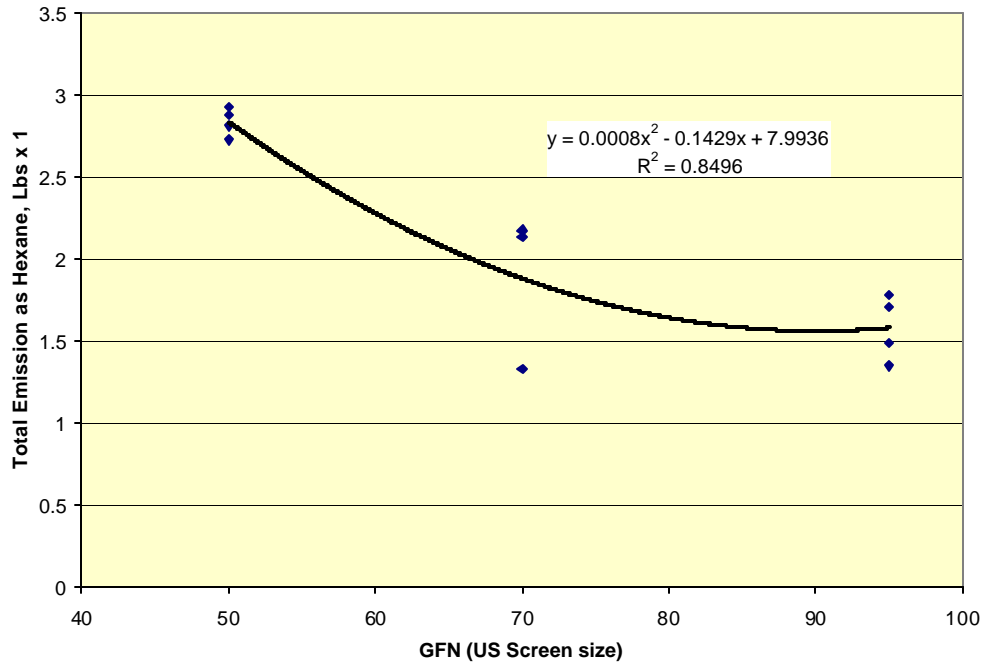


Figure 3-2 Total Emissions from Core Making vs. Core Blow Time

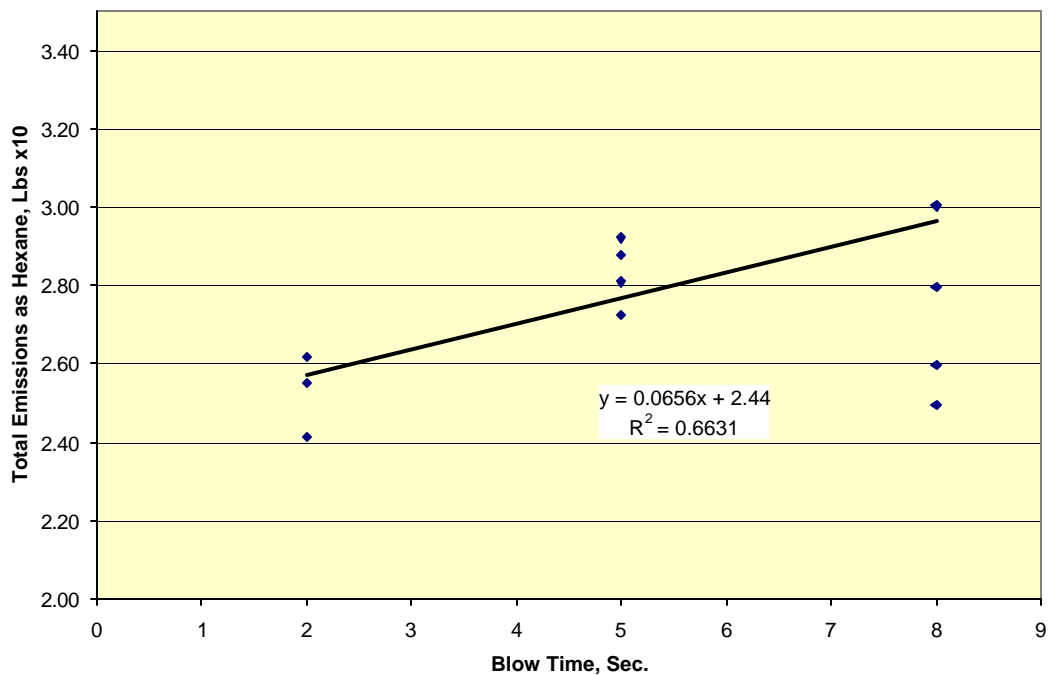


Figure 3-3 Total Emissions from Core Making vs. Sand Temperature

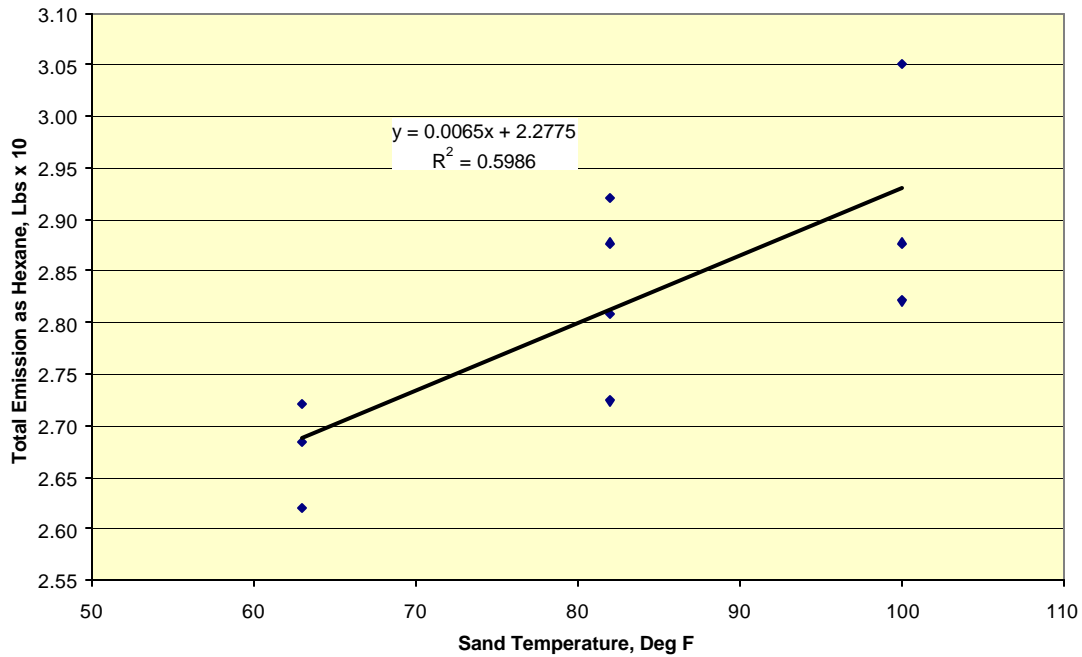


Figure 3-4 Total Emission from Core Making vs. Binder Content

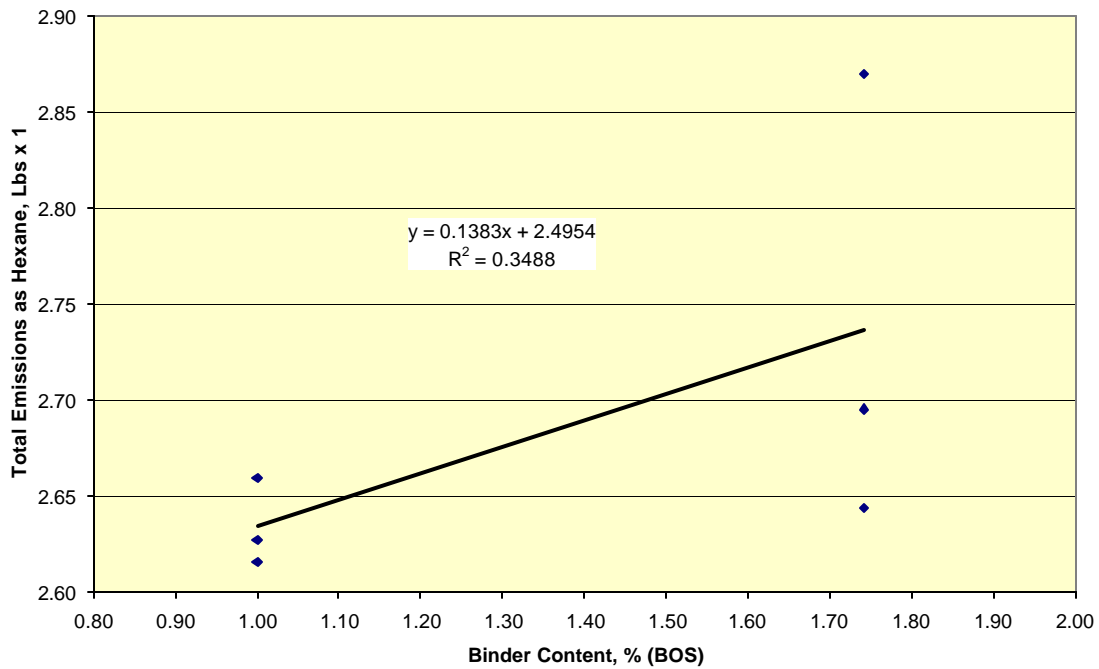


Figure 3-5 Total Emissions from Core Making vs. Purge Air Temperature

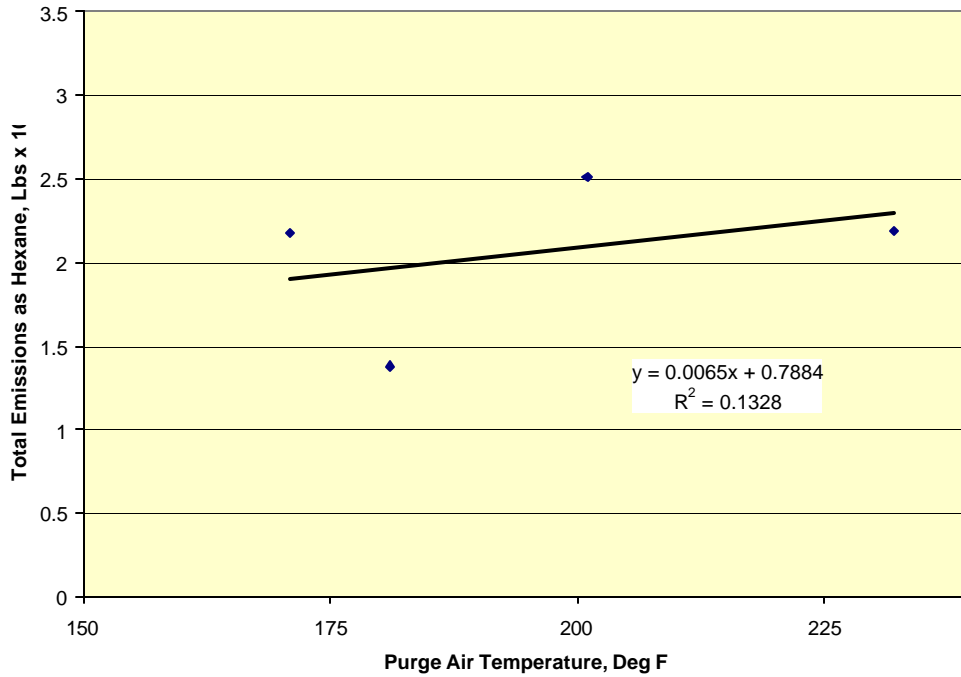


Figure 3-6 Total Emissions from Core Making vs. Purge Air Pressure

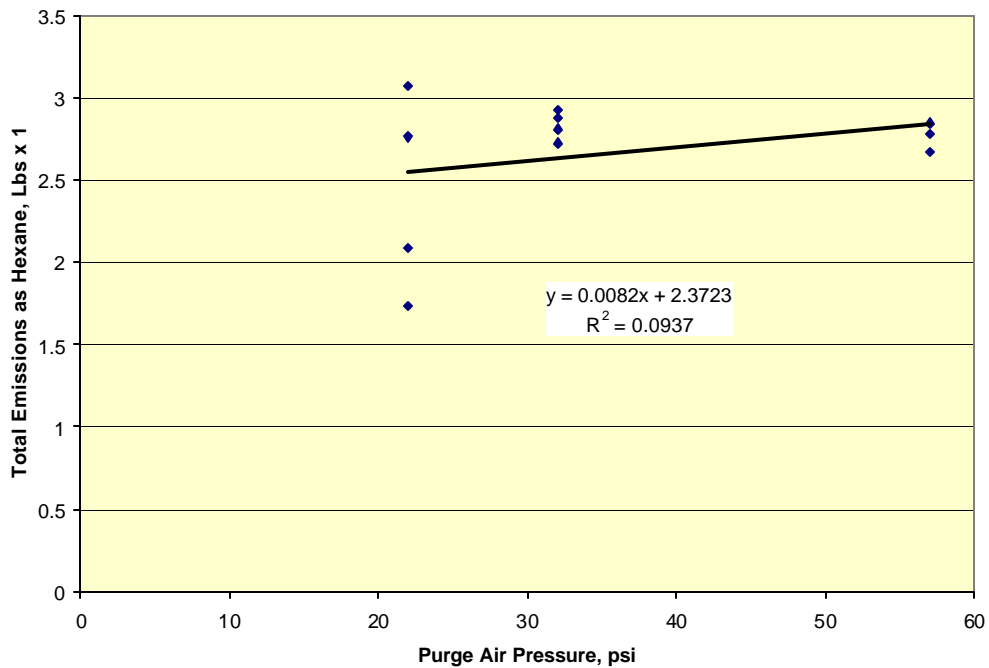


Figure 3-7 Total Emissions from Core Making vs. Purge Time

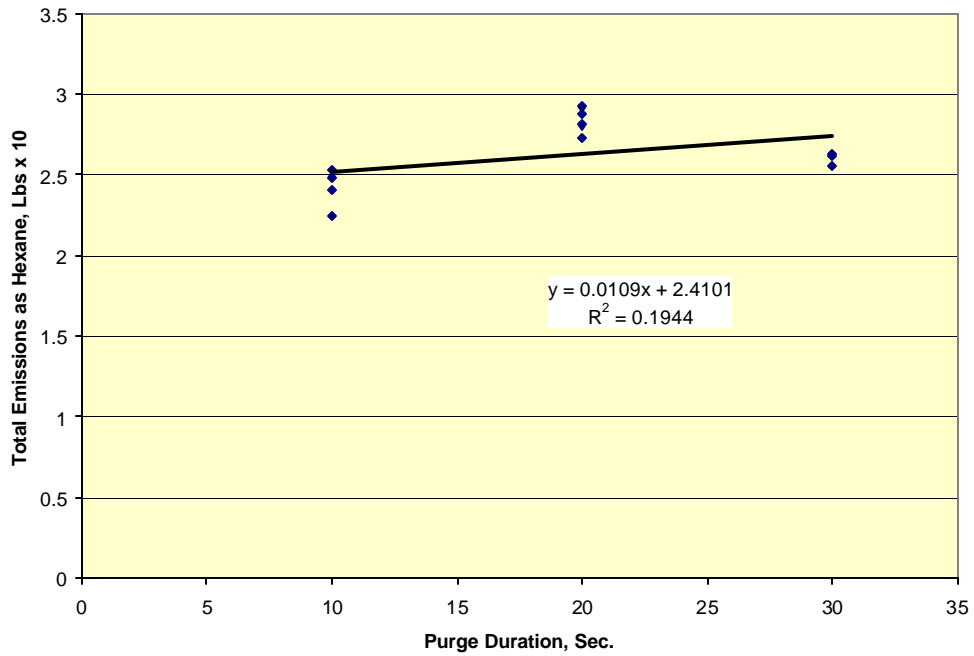


Figure 3-8 Total Emissions from Core Making vs. Blow Pressure

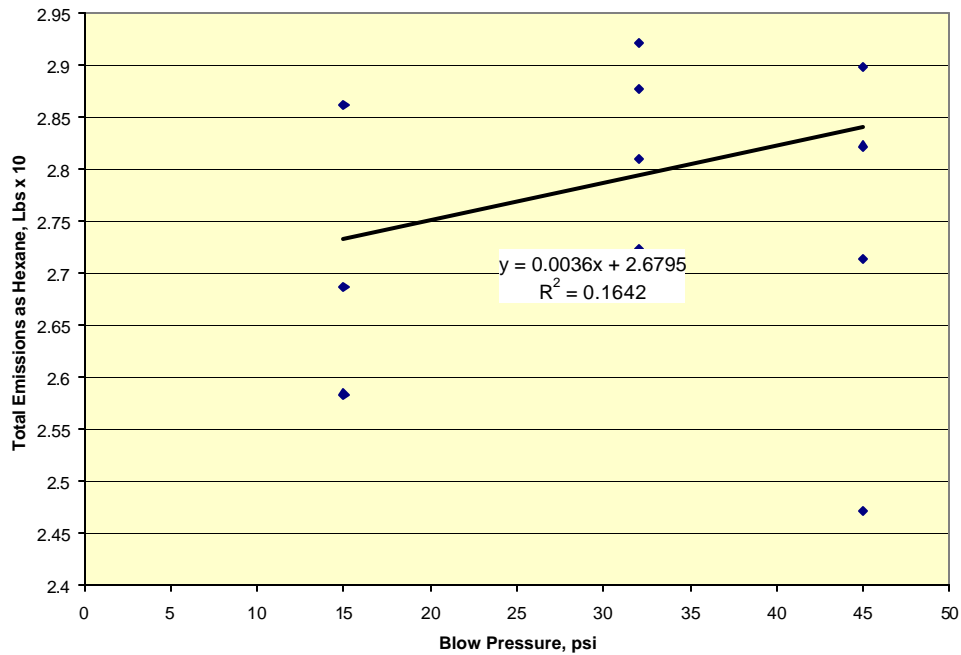


Table 3-2 Process Regression Equations and Relative Impact on Emissions

Process Event	Core Making Regression Equation Lbs x 10	Correlation Coefficient R ²	Parameter Range		Calculated Emission Lbs x 10		Emission Range for Parameter Range Lbs. x 10	Relative Emission Change Over the Parameter Range
			Low	High	Low	High		
Sand Mean Particle Size, GFN	$Y = 0.0008X^2 - 0.143X + 7.99$	0.85	50	95	2.84	1.625	-1.22	-11.6
Blow Time, Seconds	$Y = 0.065X + 2.44$	0.75	2	8	2.57	2.96	0.39	3.7
Sand Temperature, F	$Y = 0.0065X + 2.28$	0.60	63	100	2.69	2.98	0.24	2.3
Binder Content, %	$Y = 0.14X + 2.50$	0.35	1.00	1.75	2.64	2.75	0.11	1.0
Purge Temperature, F	$Y = 0.0065X + 0.79$	0.13	171	232	1.90	230	0.40	3.8
Purge Pressure, psi	$Y = 0.0082X + 2.37$	0.09	22	57	2.55	2.84	0.29	2.7
Purge Time, Seconds	$Y = 0.011X + 2.41$	0.19	10	30	2.52	2.74	0.22	2.1
Blow Pressure, psi	$Y = 0.0036X + 2.68$	0.16	15	45	2.73	2.84	0.11	1.0

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4.0 Discussion of Results

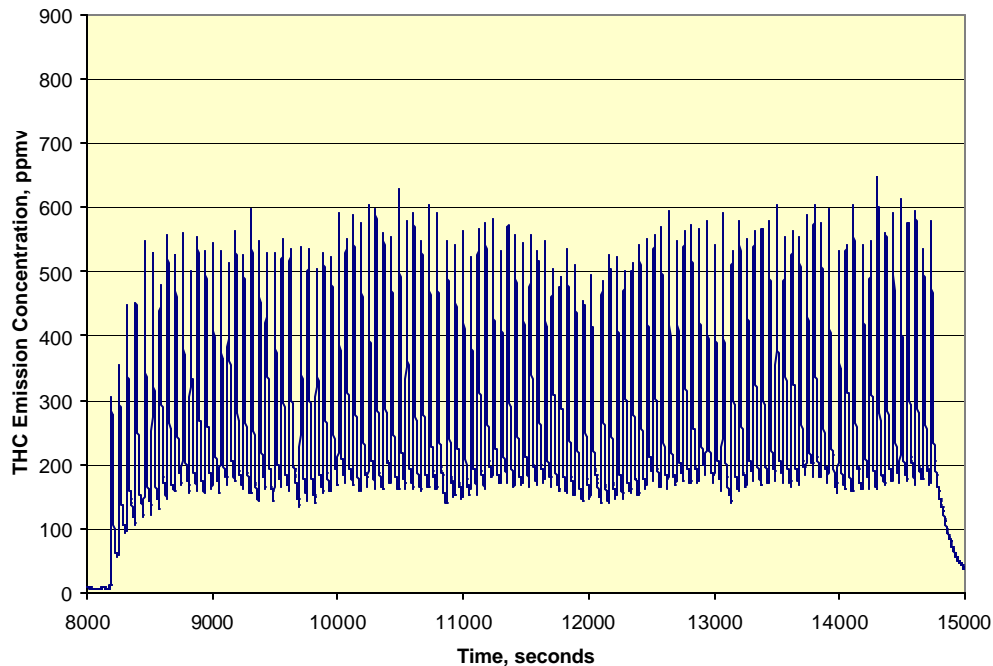
Hydrocarbon emissions as hexane based on an approved Wisconsin DNR method were measured during core making activities associated with the use of a phenolic urethane binder system in the Technikon research and development core production facility. All of the core-making measurements were conducted within enclosures meeting the criteria for a temporary total enclosure according to US EPA Method 204. Results in this report are expressed in pounds.

The HC as Hexane represents the sum of all compounds that elute from a gas chromatograph between the retention times of hexane and hexadecane.

The emission mechanism is principally sand surface evaporation of binder solvents even though some of that sand surface may be located internally in a loosely aggregated mass.

Core making (blowing) contributes the largest proportion of total core manufacturing emissions (59-72%) and core storage (21-41%) based on similarly run tests (Test FD). The gas and purge emissions were collected, as an aggregate sample from a common stack, after the process had run sufficiently for the fugitives to come to equilibrium. Equilibrium was determined from THC monitoring where the individual core cycles can be seen riding atop the fugitive background.

Figure 4-1 THC Profile for Core Blowing Process



The process variables for blowing of a Phenolic urethane core are sand temperature, binder content, blow time, blow pressure, purge air pressure, purge air temperature, purge duration, and sand particle size. Each of these were evaluated regarding their influence on the air borne emissions.

The emissions evolved during this part of the experiment come from sand materials previously subjected to the same seven (7) minute mixing criteria described in Part I: Mixing of this three part report. Testing was done in a Redford/Carver Model CB22 vertical core machine. The test piece was a standard 1-on, 7.25 pound, AFS step core. The standard process was as follows with each parameter varied one-at-a-time from this standard method:

- Sand Type: 50 GFN 4 screen Lakesand.
- Binder content: 1.0 % (BOS) of Ashland Chemical Co. Isocure® 305/904 binder mixed in a 55/45 ratio of part I/part II.
- Mixing time: 7 minutes.
- Sand Temperature: 80°F.
- Blow Time: 5 seconds.
- Blow Pressure: 30 psi.
- Purge Time: 20 seconds.
- Purge Pressure: 45 psi.
- Purge Temperature: 176°F.

The major emissions from the PU binders were caused by the evaporation of the solvents from the resin. The core blowing process includes all three physical parameters influencing evaporation: temperature, effective exposed surface area, and air movement over the surface of the coated sand grains.

Core making by mechanized blowing is a multi-step set of processes. The previously mixed sand is pneumatically injected into the core box causing the sand bulk volume and apparent surface to be momentarily increased several fold. Heated “blow” air permeates the liquid-coated, initially loose, granular mass to vents in the core box. Once in place the liquid binder components were cured into a rigid mass by percolation of the catalyst Triethylamine (TEA). The core in the core box was then purged with heated air to remove most of the volatile solvents and the catalyst TEA by permeating the geometrically fixed solid core. Some of the volatile solvents are retained on internal sand surfaces others are temporarily trapped in the rigid binder. Both are carried with the core to storage.

The primary direct emission drivers were demonstrated to be the mean sand particle size (GFN), the blow duration, and the sand temperature. See Table 3-2.

As was learned in the Mixing section (Part I) of this report the sand temperature is the primary driver for the evaporation process because temperature raises the vapor pressure of the solvents.

The blow time reflects the duration of time when the sand is loosely aggregated and when air can freely pass through the sand contacting most of the apparent coated surface to purge emissions. The core, once formed, has much less apparent surface area.

The ability of the purged air to pass through the core and scavenge emissions is dependent on the open voids between the sand grains. The sand particle sizing and distribution defines the open voids. In general the smaller the mean particle size, high GFN number, the more resistance to air passing through the core. Additionally with smaller voids between the sand grains a given thickness of liquid binder will occlude those voids making them less permeable to the passage of purging air.

Secondary drivers were identified to be all of the other above mentioned measured parameters because of their influence on the air movement over and through the sand and thus on the amount of apparent exposed surface. The emitting sand surface is both the core surface and the inter-granular voids.

The experimental confidence levels are very low for the secondary drivers being separable causes for emissions.

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APPENDIX A APPROVED TEST PLAN FOR TEST EU

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TECHNIKON TEST PLAN

- > **CONTRACT NUMBER:** 1409 **TASK NUMBER:** 1.3.1
- > **WORK ORDER NUMBER:** 1169 **Series:** EU
- > **SAMPLE EVENTS:** 8 TGOC preliminary, 9 mix, 51 make , 17 store TGOC & tubes
- > **SITE:** PRE-PRODUCTION(243) X **FOUNDRY(238)**
- > **TEST TYPE:** Core mixing, core making, core storage. Process variables study.
- > **METAL TYPE:** None
- > **MOLD TYPE:** None
- > **NUMBER OF TESTS:** 5 Preliminary, 9 core sand mixing, 17 core-making with scratch hardness, 17 core-storage: All in triplicate.
- > **CORE TYPE:** AFS Step Core, Ashland ISOCURE® 305/904 phenolic urethane binder at 1.0% and 1.4% and 1.75% total resin, 55% Part I, 45% part II, TEA gas catalyzed.
- > **TEST DATE:** **START:** 4 Nov 2002
FINISHED: 12 Dec 2002

TEST OBJECTIVES:

1. Measure VOCs and HAPs from Core Mixing, Core Making & Core Storage by the methods established in the **Core Mix, Make, & Store Baseline 2002** from a regiment of tests in each venue which explore the range of process variation normally encountered in commercial foundry practice.

VARIABLES :

1. **Preliminary Tests:** The first tests will include a battery to outline the process sensitivity to the operating environment and define a stable region of testing. This series will include heat gain from gear and sand friction, emission sampling rate, environmental temperature, and mixer fullness for each condition.
2. **Core Sand Mixing:** The Mixing parameters will include sand GFN, sand temperature, binder concentration, and mixing speed. The reference uncoated sand shall be Wexford W450 Lakesand. It shall be preheated or cooled to a reference temperature of 80 +/-2 degrees Fahrenheit. The reference binder concentration shall be 1.4 +/-0.014% Ashland ISOCURE® 305/904 mixed Part I/Part II in the ratio of 55/45. The sand will be coated in a Redford/Carver 50 pound core sand mixer for 7 minutes. One minute shall be used to dispense the sand and the two binder components and one additional minute shall be used

strictly for discharging the mixer. Each core sand-mixing test shall be three (3) seven (7)-minute 50 pound cycles, monitored continuously by TGOC and adsorption tubes. Prior to the first mixing test five (5) batches shall be run to normalize the background within the muller. Sampling media will be changed after each three-cycle test during which time mixing will continue in order to maintain the background concentration. A total of three (3) mixing cycles shall be run at each of 3 parameter levels for each variable.

3. **Core Making:** The Make tests will each include effects of sand temperature, binder content, blow time, blow pressure, purge pressure, purge air temperature, purge duration, & sand GFN with sand mixed to a standard duration, sand temperature, binder content, and/or ambient (enclosure) air temperature as called out in the attached test plan tables. Make tests will include scratch hardness testing at 2 hours age. The Redford/Carver core machine will operate on a nominal one (1) minute door-to-door cycle. The environmental enclosure shall be supplied with air controlled to 82 +/- 5 degrees Fahrenheit. TEA will be fed to the core machine at a nominal 5 grams per cycle. The reference purge pressure shall be 45 +/- 2 psi for 20 seconds. Reference blow pressure shall be 30 psi. The core-make test will begin after the core machine has run sufficient time, at rate, to have the background emission concentration stabilize. Each core-make test will be 30 core cycles, about one half hour long, with continuous TGOC and adsorption tube sampling. Sample media will be changed after each 30 cycle test. The core machine will run continuously during media change and testing to maintain the background concentration. The gas & purge and fugitive emissions will be collected to a common sampling stack. Each core will be weighed.
4. **Core Storage:** The storage test will consist of weighed cores sequentially sampled, four (4) in a group, from the core machine during the make test and placed in individual sampling domes. The domes are in a temperature controlled room at 82 +/- 5 degrees Fahrenheit and sampled continuously with TGOC and adsorption tubes for 1.5 hours.

BRIEF OVERVIEW:

Core making is not a single process but rather a series of steps each with its own process collectable and fugitive emissions. This test will look at selected HAP & VOC emissions from combined process collectable and fugitive emission streams during each of the core sand mixing, core making, and core storage steps. Each step will have a series of parameters varied per the attached test plan tables while all other controllable parameters are held in reference value ranges.

SPECIAL CONDITIONS:

The sand mixer will have a removable lid that allows air to infiltrate radially from the perimeter. Materials will be charged through a closeable door in the lid. Samples will be extracted from the center of the headspace below the lid. The mixer shall be surrounded on 4 sides with an insulating wall that extends 3 inches above the mixer to reduce room ambient influences. The enclosure

shall be flooded with air controlled to the reference temperature range. The emission samples shall be extracted at a reference rate.

The core machine with step core tooling shall be housed in a double walled emission enclosure. The area between the walls shall be flushed with temperature controlled air at 82+/-5 degrees Fahrenheit. This air shall be the ambient make up air for the core process within the enclosure. The core box and core machine shall be tightly plumbed to extract gasses passed through the core box into a common sampling stack with the fugitive gasses. The sampling environment will be maintained at 75-85°F. Core storage will be individual cores tested under individual glass domes in groups of four (4) cores for a period of 1.5 hours. The environment will be totally captured. One dome will be monitored by TGOC.

_____ Process Engineering Manager (Technikon)	_____ Date
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_____ V.P. Measurement Technology (Technikon)	_____ Date
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_____ V.P. Operations (Technikon)	_____ Date
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_____ Test Design Committee Representative	_____ Date
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_____ Emission Committee Representative	_____ Date
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APPENDIX B SUMMARY TABLES FOR CHART DATA

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Table B-1 Core Making Process Parameter Matrix

EU Core Make & Store Process Variables Summary (page 1)

Test No.	Test Date	Test Purpose	Make Sample No.	Make Emission Weight Lbs x 10	Store Sample No.	Store Emission Weight Lbs. x 1000	Sand Type	Sand Weight Lbs	Sand Temp F	Binder Content % (BOS)	Ambient Fdry Air Temp F	Probe Air Temp F	Blow Time Sec.	Blow Press psi	Purge Air Press psi	Purge Air Temp F	Purge Air Duration Sec.
Mk2a1	11/26/02	Emission vs low sand temp	EU201	2.721	EU301	1.3	W450	50	63	0.98	66	80	5	30	45	176	20
Mk2a2	11/26/02	Emission vs low sand temp	EU202	2.620	EU302	1.2	W450	50	63	0.98	66	80	5	30	45	176	20
Mk2a3	11/26/02	Emission vs low sand temp	NA	NA	Dup	0.9	W450	50	63	0.98	66	80	5	30	45	176	20
Mk2a3	11/26/02	Emission vs low sand temp	EU203	2.685	EU303	1.2	W450	50	63	0.98	66	80	5	30	45	176	20
Mk2b1	11/26/02	Emission vs mid sand temp	EU204	2.877	EU304	1.4	W450	50	82	0.98	68	83	5	30	45	176	20
Mk2b1	11/26/02	Emission vs mid sand temp	EU205	2.809	EU305	1.1	W450	50	82	0.98	69	83	5	30	45	176	20
Mk2b2	11/26/02	Emission vs mid sand temp	Dup	2.724	NA	NA	W450	50	82	0.98	69	83	5	30	45	176	20
Mk2b3	11/26/02	Emission vs mid sand temp	EU206	2.921	EU306	1.1	W450	50	82	0.98	69	83	5	30	45	176	20
Mk2c1	11/26/02	Emission vs high Sand temp	EU207	2.821	EU307	1.3	W450	50	100	0.98	69	80	5	30	45	176	20
Mk2c2	11/26/02	Emission vs high Sand temp	NA	NA	Dup	1.1	W450	50	100	0.98	69	80	5	30	45	176	20
Mk2c2	11/26/02	Emission vs high Sand temp	EU208	2.877	EU308	1.4	W450	50	100	0.98	69	80	5	30	45	176	20
Mk2c3	11/26/02	Emission vs high Sand temp	EU209	3.050	EU309	1.7	W450	50	100	0.98	70	80	5	30	45	176	20
Mk1a1	12/02/02	Emission vs Lo% binder	EU210	2.615	EU310	1.6	W450	50	82	1.00	64	84	5	30	45	176	20
Mk1a2	12/02/02	Emission vs Lo% binder	EU211	2.659	EU311	1.5	W450	50	80	1.00	64	84	5	30	45	176	20
Mk1a2	12/02/02	Emission vs Lo% binder	NA	NA	Dup	1.0	W450	50	80	1.00	64	84	5	30	45	176	20
Mk1a3	12/02/02	Emission vs Lo% binder	EU212	2.627	EU312	1.3	W450	50	83	1.00	65	84	5	30	45	176	20
Mk1b1	12/02/02	Emission vs Hi% binder	EU213	2.643	EU313	2.0	W450	50	82	1.74	65	84	5	30	45	176	20
Mk1b2	12/02/02	Emission vs Hi% binder	EU214	2.695	EU314	2.1	W450	50	83	1.74	66	84	5	30	45	176	20
Mk1b3	12/02/02	Emission vs Hi% binder	EU215	2.870	EU315	2.0	W450	50	83	1.74	67	84	5	30	45	176	20
Mk3a1	12/03/02	Emission vs Mid Blow time	EU216	2.413	EU316	1.4	W450	50	80	0.98	70	84	2	32	45	176	20
Mk3a1	12/03/02	Emission vs Mid Blow time	NA	NA	Dup	1.0	W450	50	80	0.98	70	84	2	32	45	176	20
Mk3a2	12/03/02	Emission vs Mid Blow time	EU217	2.552	EU317	1.3	W450	50	79	0.98	70	84	2	32	45	176	20
Mk3a3	12/03/02	Emission vs Mid Blow time	EU218	2.619	EU318	1.3	W450	50	82	0.98	71	84	2	32	45	176	20
Mk3b1	12/6/02	Emission vs hi Blow time	EU219	2.595	EU319	1.2	W450	50	83	0.98	62	82	8	32	45	176	20
Mk3b2	12/6/02	Emission vs hi Blow time	EU220	2.495	EU320	1.2	W450	50	80	0.98	63	82	8	32	45	176	20
Mk3b2	12/6/02	Emission vs hi Blow time	Dup	2.797	Dup	0.9	W450	50	80	0.98	63	82	8	32	45	176	20
Mk3b3	12/6/02	Emission vs hi Blow time	EU221	3.003	EU321	1.2	W450	50	82	0.98	64	82	8	32	45	176	20
Mk4a1	12/3/02	Emission vs mid blow pres	EU222	2.687	EU322	1.4	W450	50	80	0.98	63	81	5	15	45	176	20
Mk4a2	12/3/02	Emission vs mid blow pres	EU223	2.584	EU323	1.3	W450	50	79	0.98	64	81	5	15	45	176	20
Mk4a3	12/3/02	Emission vs mid blow pres	EU224	2.861	EU324	1.3	W450	50	83	0.98	65	81	5	15	45	176	20
Mk4a3	12/3/02	Emission vs mid blow pres	NA	NA	Dup	1.1	W450	50	83	0.98	65	81	5	15	45	176	20
Mk4b1	12/3/02	Emission vs hi blow pres	EU225	2.714	EU325	1.6	W450	50	80	0.98	66	82	5	45	45	176	20
Mk4b1	12/3/02	Emission vs hi blow pres	Dup	2.822	NA	NA	W450	50	80	0.98	66	82	5	45	45	176	20
Mk4b2	12/3/02	Emission vs hi blow pres	EU226	2.897	EU326	1.4	W450	50	83	0.98	67	82	5	45	45	176	20
Mk4b3	12/3/02	Emission vs hi blow pres	EU227	2.472	EU327	1.5	W450	50	83	0.98	68	82	5	45	45	176	20

Table B-1 Core Making Process Parameter Matrix (continued)

EU Core Make & Store Process Variables Summary (page 2)

Test No.	Test Date	Test Purpose	Make Sample No.	Make Emission Weight Lbs x 10	Store Sample No.	Store Emission Weight Lbs. x 1000	Sand Type	Sand Weight Lbs	Sand Temp F	Binder Content % (BOS)	Ambient Fdry Air Temp F	Probe Air Temp F	Blow Time Sec.	Blow Press psi	Purge Air Press psi	Purge Air Temp F	Purge Air Duration Sec.
Mk5a1	12/4/02	Emission vs Lo Purge pres	EU228	2.087	EU328	1.9	W450	50	83	0.98	61	84	5	32	22	176	20
Mk5a2	12/4/02	Emission vs Lo Purge pres	EU229	1.732	EU329	1.7	W450	50	80	0.98	62	84	5	32	22	176	20
Mk5a3	12/4/02	Emission vs Lo Purge pres	EU230A	2.761	EU330a	1.6	W450	50	81	0.98	69	84	5	32	22	176	20
Mk5a3	12/4/02	Emission vs Lo Purge pres	Dup	3.067	NA	NA	W450	50	81	0.98	65	84	5	32	22	176	20
Mk5b1	12/4/02	Emission vs Mid Purge pres	EU231	2.845	EU331	1.4	W450	50	80	0.98	65	85	5	32	57	176	20
Mk5b2	12/4/02	Emission vs Mid Purge pres	EU232	2.781	EU332	1.3	W450	50	79	0.98	66	85	5	32	57	176	20
Mk5b2	12/4/02	Emission vs Mid Purge pres	NA	NA	EU332	0.9	W450	50	79	0.98	67	85	5	32	57	176	20
Mk5b3	12/4/02	Emission vs Mid Purge pres	EU233	2.669	EU333	1.1	W450	50	82	0.98	67	85	5	32	57	176	20
Mk6a1	12/17/02	Emission vs Purge temp	EU234A	2.174	EU334A	1.5	W450	50	81	0.98	63	82	5	32	45	171	20
Mk6a2	12/17/02	Emission vs Purge temp	EU235	2.508	EU335a	1.2	W450	50	78	0.98	64	82	5	32	45	201	20
Mk6a3	12/17/02	Emission vs Purge temp	EU236	2.186	EU336a	0.8	W450	50	80	0.98	65	82	5	32	45	232	20
Mk6a3	12/17/02	Emission vs Purge temp	NA	NA	Dup	0.4	W450	50	80	0.98	65	82	5	32	45	232	20
Mk6b3	12/17/02	Emission vs Purge temp	EU237	1.382	EU337	0.9	W450	50	79	0.98	66	79	5	32	45	181	20
	12/17/02	Emission vs Purge temp	NA	NA	EU338	0.9	W450	50	82	0.98	66	79	5	32	45	----	20
	12/17/02	Emission vs Purge temp	NA	NA	EU339	0.8	W450	50	80	0.98	66	79	5	32	45	----	20
	12/17/02	Emission vs Purge temp	NA	NA	Dup	0.7	W450	50	80	0.98	66	79	5	32	45	----	20
Mk7a1	12/9/02	Emission vs short Purge dur	EU240	2.241	EU340	1.2	W450	50	80	0.98	62	82	5	32	45	176	10
Mk7a2	12/9/02	Emission vs short Purge dur	EU241	2.409	EU341	1.3	W450	50	82	0.98	63	82	5	32	45	176	10
Mk7a2	12/9/02	Emission vs short Purge dur	Dup	2.531	EU341	NA	W450	50	82	0.98	63	82	5	32	45	176	10
Mk7a3	12/9/02	Emission vs short Purge dur	EU242	2.486	EU342	3.0	W450	50	80	0.98	64	82	5	32	45	176	10
Mk7b1	12/9/02	Emission vs long Purge dur	EU243	2.658	EU343	1.1	W450	50	80	0.98	64	82	5	32	45	176	30
Mk7b2	12/9/02	Emission vs long Purge dur	EU244	2.618	EU344	1.0	W450	50	81	0.98	64	82	5	32	45	176	30
Mk7b3	12/9/02	Emission vs long Purge dur	EU245	2.550	EU345	1.1	W450	50	80	0.98	65	82	5	32	45	176	30
Mk7b3	12/9/02	Emission vs long Purge dur	Dup	2.634	NA	NA	W450	50	80	0.98	65	82	5	32	45	176	30
Mk8a1	12/18/02	Emission vs lo GFN	EU246A	2.175	EU346	3.0	A70	50	77	1.75	60	82	5	30	45	176	20
Mk8a2	12/18/02	Emission vs lo GFN	EU247	2.135	EU347	2.3	A70	50	77	1.75	60	82	5	30	45	176	20
Mk8a3	12/18/02	Emission vs lo GFN	EU248	1.327	EU348	2.2	A70	50	77	1.75	60	82	5	30	45	176	20
Mk8b1	12/18/02	Emission vs hi GFN	EU249	1.486	EU349	2.7	F-95	50	75	1.75	63	83	5	30	45	176	20
Mk8b1	12/18/02	Emission vs hi GFN	NA	NA	Dup	2.3	F-95	50	75	1.75	63	83	5	30	45	176	20
Mk8b2	12/18/02	Emission vs hi GFN	EU250	1.347	EU350-	2.9	F-95	50	75	1.75	64	83	5	30	45	176	20
Mk8b2	12/18/02	Emission vs hi GFN	Dup	1.775	NA	NA	F-95	50	75	1.75	64	83	5	30	45	176	20
Mk8b3	12/18/02	Emission vs hi GFN	EU251	1.709	EU351	3.1	F-95	50	75	1.75	64	83	5	30	45	176	20

APPENDIX C GLOSSARY

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Glossary

ACFM	Actual Cubic Feet Per Minute
BO	Based on ().
BOS	Based on Sand.
HAP	Hazardous Air Pollutant defined by the 1990 Clean Air Act Amendment
HC as Hexane	Calculated by the summation of all area between elution of Hexane through the elution of Hexadecane. The quantity of HC is performed against a five-point calibration curve of Hexane by dividing the total area count from C6 through C16 to the area of Hexane from the initial calibration curve.
I	Invalid, Data rejected based on data validation considerations
NA	Not Applicable
ND	Non-Detect
NT	Not-Done, Lab testing was not done
POM	Polycyclic Organic Matter (POM) including Naphthalene and other compounds that contain more than one benzene ring and have a boiling point greater than or equal to 100 degrees Celsius.
PPMV	Parts Per Million by Volume
TGOC	Total Gaseous Organic Carbon
TGOC as Propane	Weighted to the detection of more volatile hydrocarbon species, beginning at C1 (methane), with results calibrated against a three-carbon alkane (propane).
VOC	Volatile Organic Compound